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Which deoiling technologies to choose for Upstream Oil and Gas applications? A multi-criteria approach

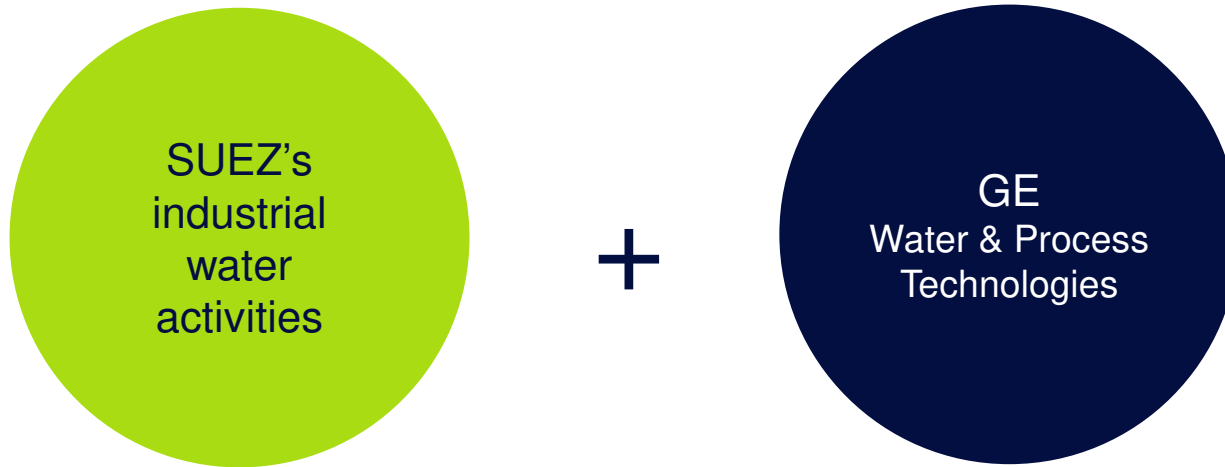
Camille Sagne - Global Technology Leader O&G
Suez Water Technologies & Solutions

Michael Cavill – Deputy Chief Technology Officer
Suez Oil & Gas Systems



**today, we are introducing
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joining forces in SUEZ



The combination of GE Water & Process Technologies' and SUEZ's industrial water activities enables SUEZ to strengthen its position as a **worldwide resource** (water and waste) **technology and solutions leader for industry**, dedicated to improve our customers' economic and environmental performance

Introduction

- **Several Conventional Technologies are available for deoiling in upstream and downstream**
- **Tighter outlet requirements → Emerging technologies, especially membrane-based technologies**
- **Different features leading to different benefits**

Which treatment line for which situation?

Content

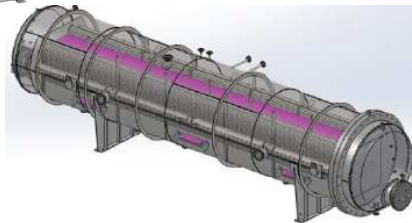
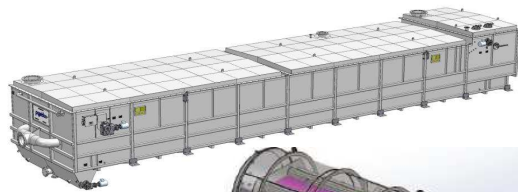
- 01 | Deoiling Technologies Overview**
- 02 | Basis for treatment line comparison**
- 03 | Multi-criteria comparison**
- 04 | Conclusion**

Deoiling Technologies Overview

Primary Separation

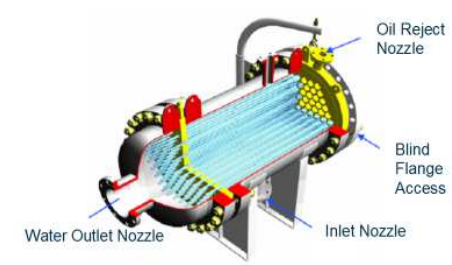
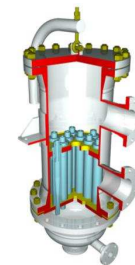
By Gravity API/CPI/VOWS

- Inlet range: 1000 – 5000 ppm
- Outlet range: 100 – 300 ppm
- No moving part, robust
- Oil recovery
- Large footprint
- Limited performances



By centrifugal forces Hydrocyclones

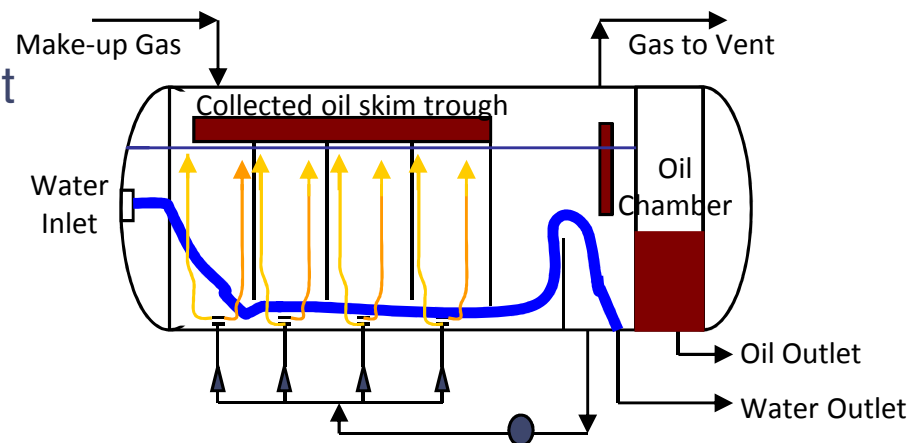
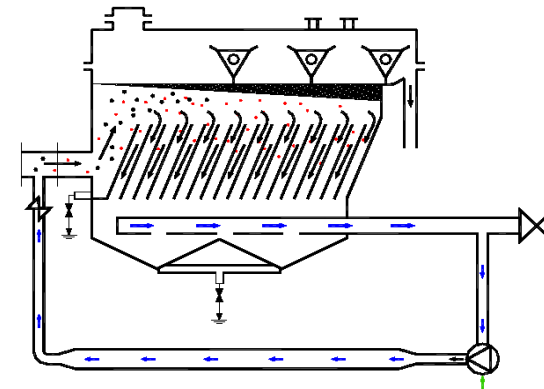
- Inlet range: 1000 – 2000 ppm
- Outlet range: 20 – 50 ppm
- Compact
- Oil recovery
- High performances
- Oil and TSS removal cannot be combined
- High pressure



Secondary Separation

By Flotation IGF/DNF

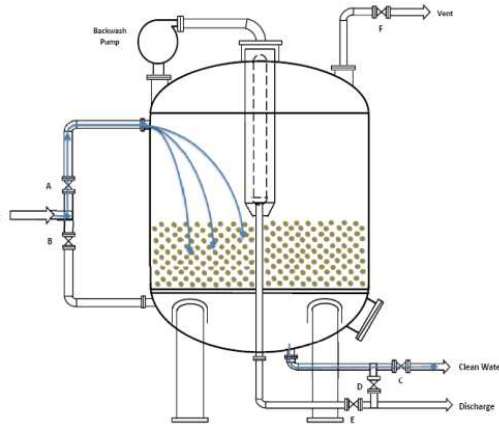
- Inlet range: 100 – 500 ppm
- Outlet range: 15 – 30 ppm
- Good performances
- Atmospheric/Low pressure
- Chemical required
- Oil recovery more difficult



Polishing

By Media Filtration NSF

- Inlet range: 15 – 50 ppm
- Outlet range: 5 – 30 ppm
- Good performances
- Not absolute cut-off
- Requires Backwash



By Membrane Filtration Ultrafiltration

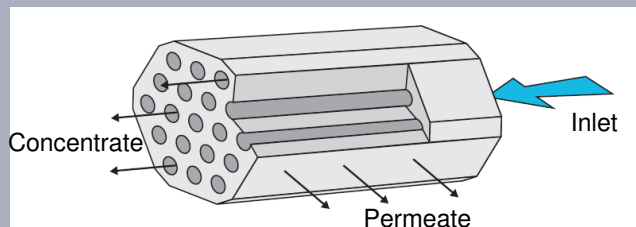
- Inlet range: 50 – 300 ppm
- Outlet range: 1 – 5 ppm
- High water quality
- Controlled particle size
- Requires Backwash/Cleaning



Membrane type and Configuration

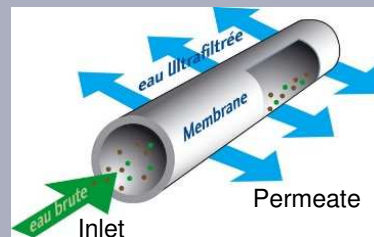
Ceramic Tubular

- High temperature and chemical resistance
- High flux
- Cross-flow



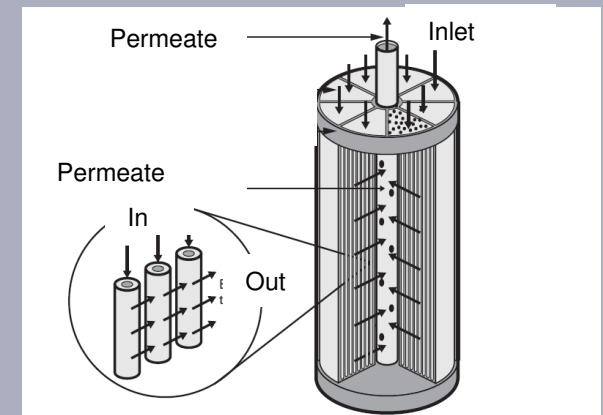
Polymeric Tubular

- Moderate temperature and chemical resistance
- High flux
- Cross-flow



Polymeric Hollow Fiber

- Lower temperature resistance
- Lower flux
- Semi dead-end



Technical evaluation through R&D program in the CIRSEE

- Extensive program → Evaluation of more than 10 different membranes
- Assessment based on several criteria including filtration performances, fouling propensity, robustness...
- Case studies based on the findings of the program

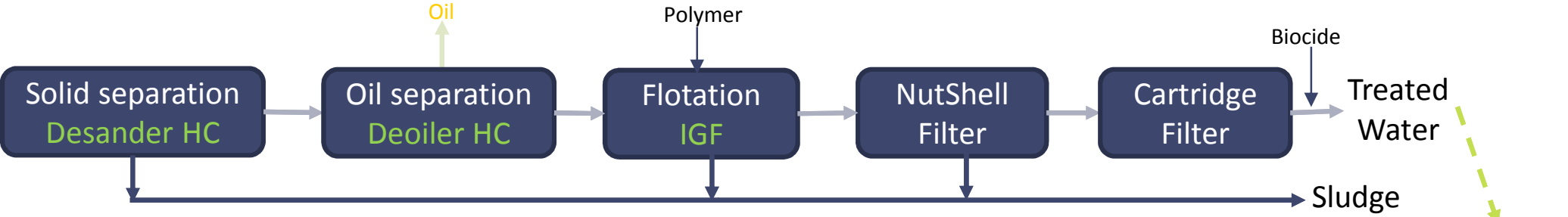


Basis for treatment line comparison

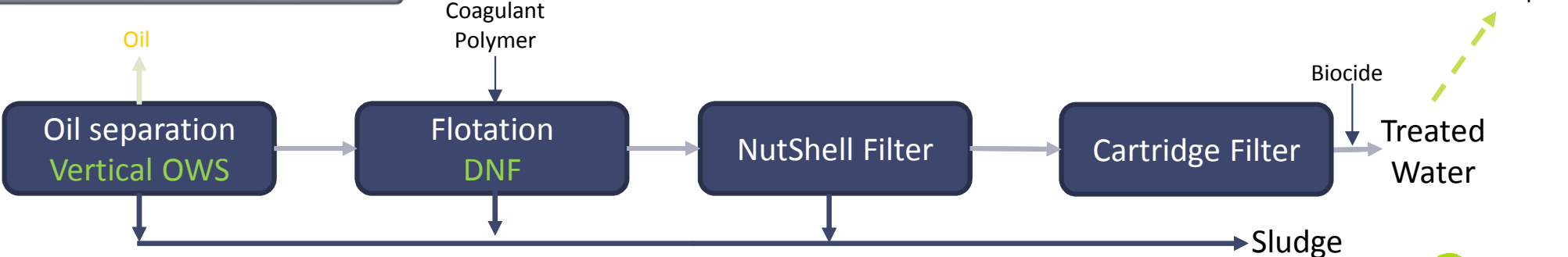
Treatment schemes for tight outlet specification

Conventional Upstream

Oil/Solid separation
Skim tank, CPI



Conventional Downstream

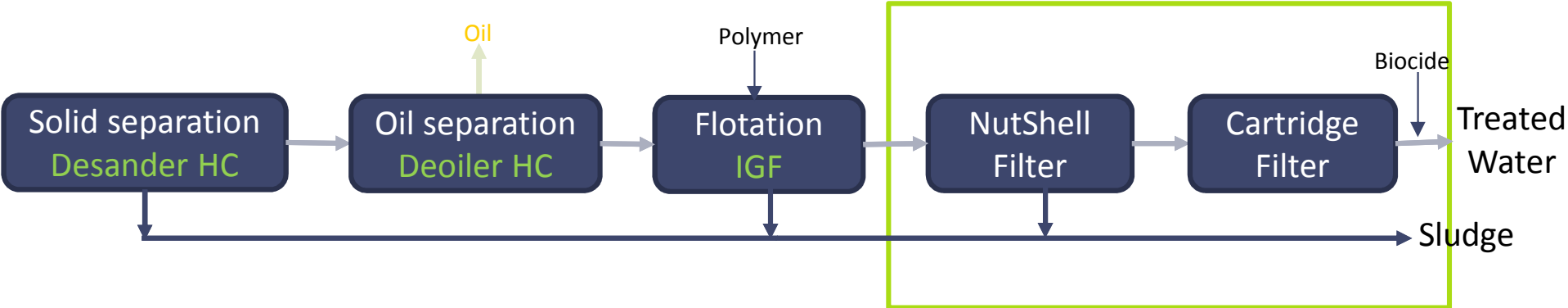
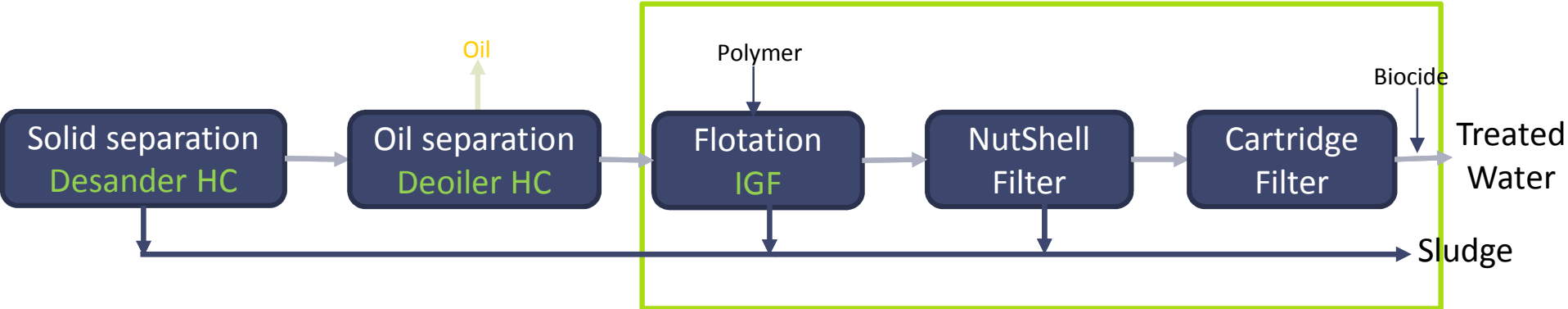


Oil: 5 ppm
TSS < 1 ppm
TSS < 1 μm



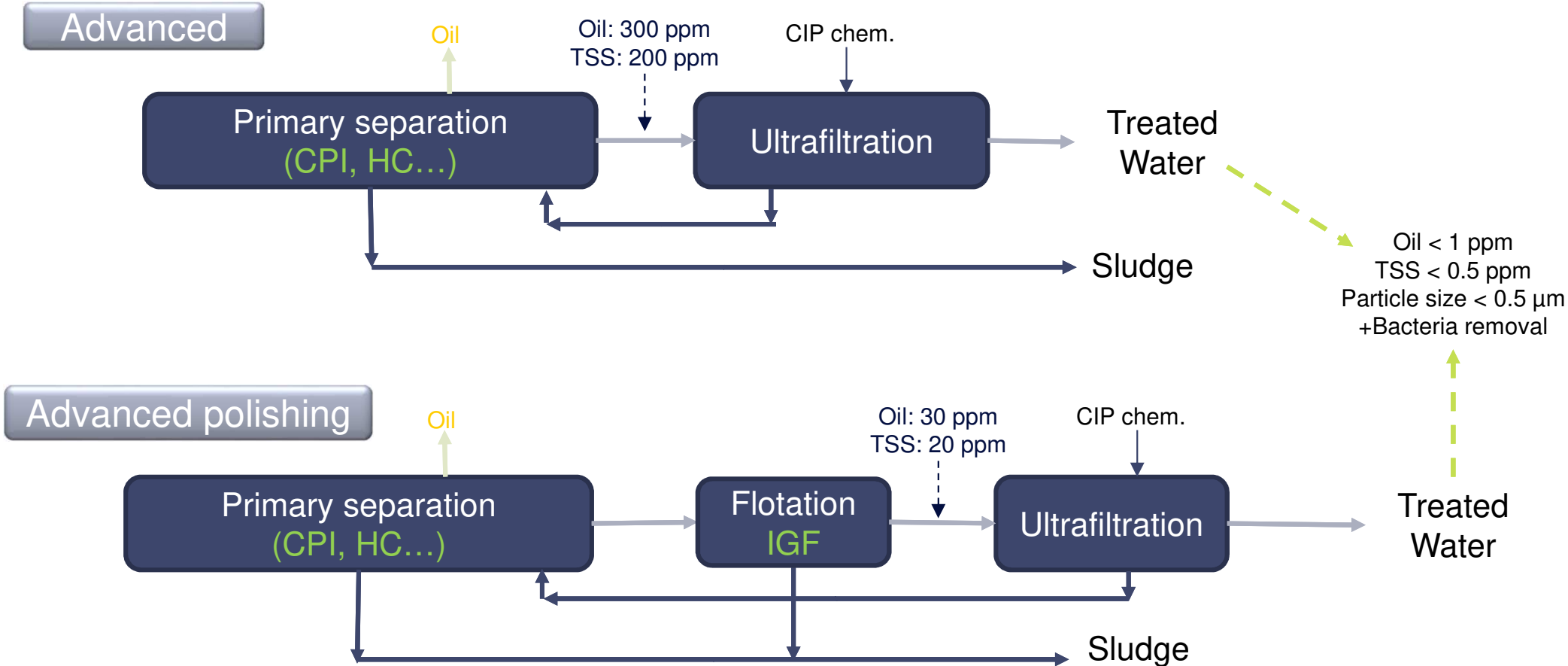
Treatment schemes for tight outlet specification

2 potential configurations



Treatment schemes for tight outlet specification

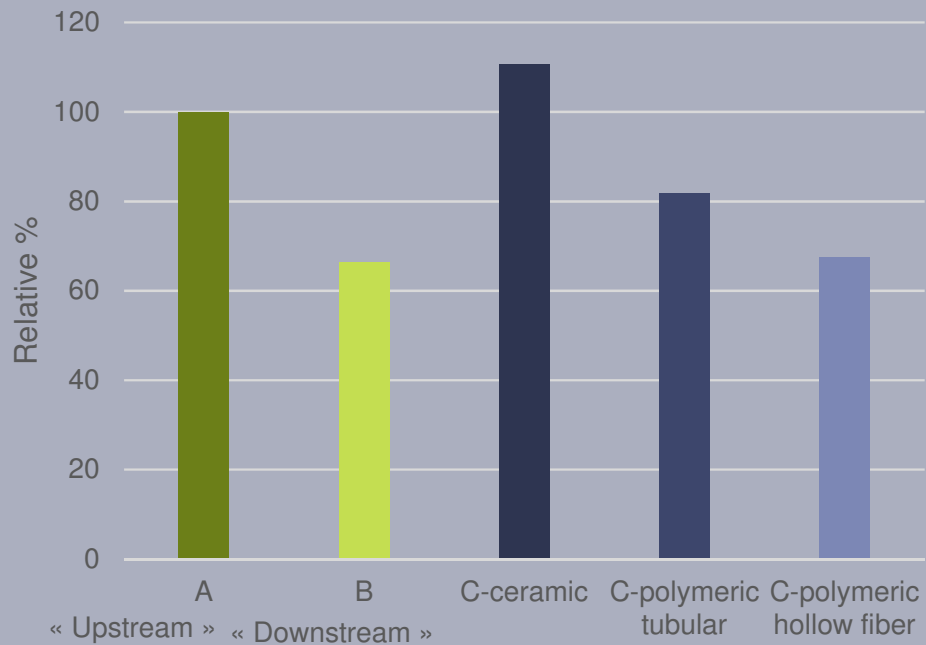
2 potential configurations



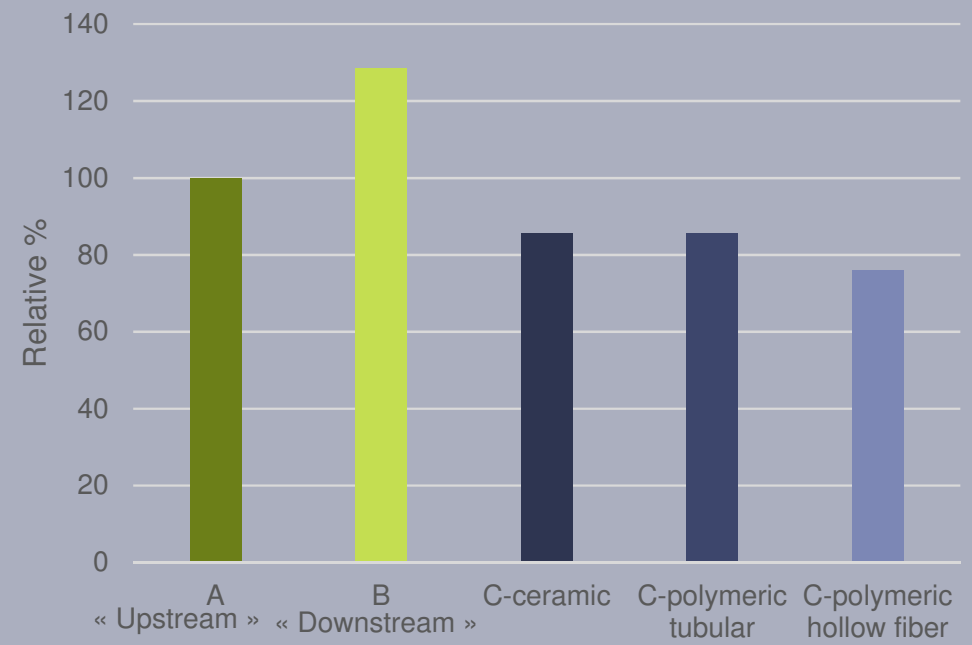
Treatment Line Comparison

CAPEX and Footprint evaluation for 2000 m³/d

Relative CAPEX

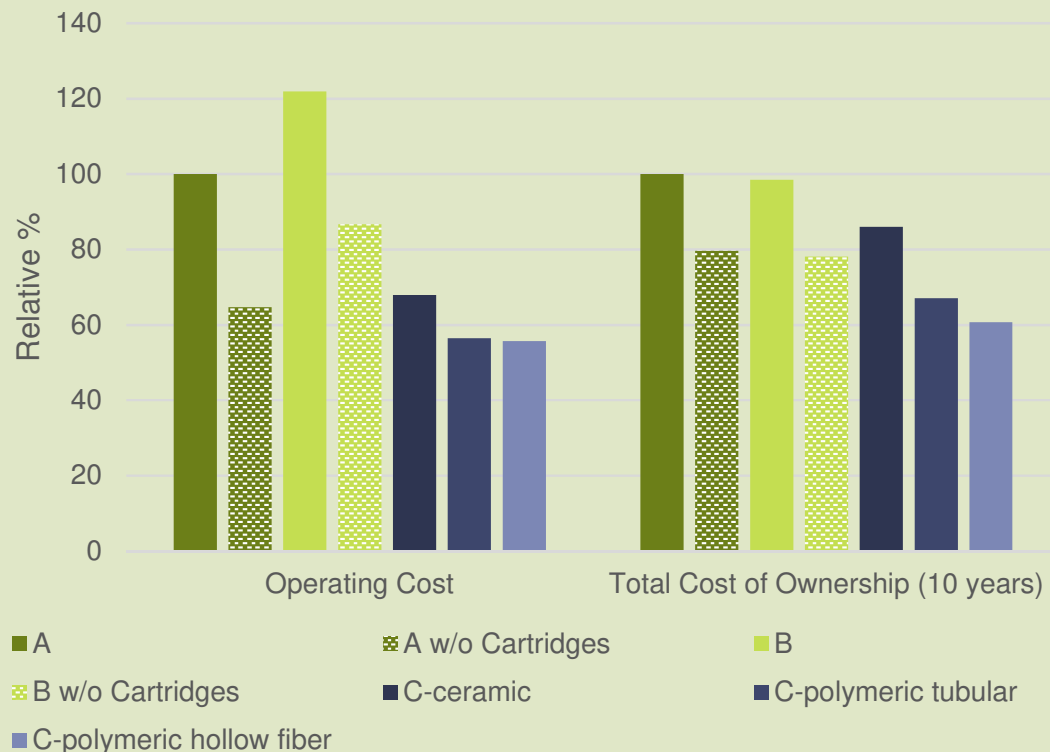


Relative Footprint



OPEX and main outcomes for 2000 m³/d

Relative OPEX and TCO

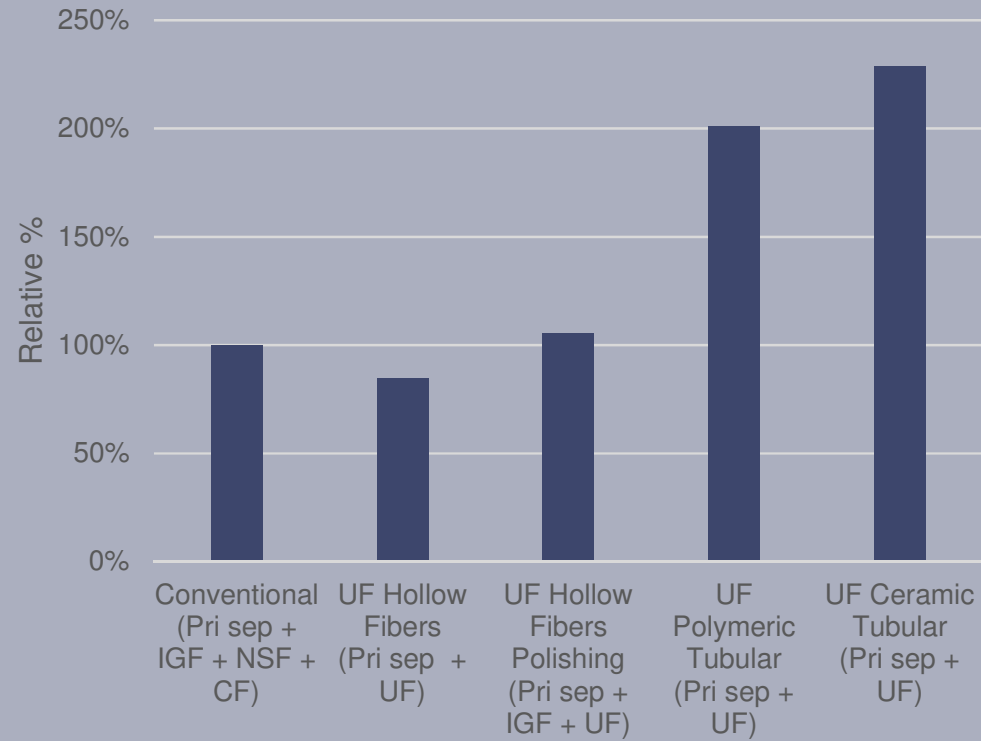


At low flow:

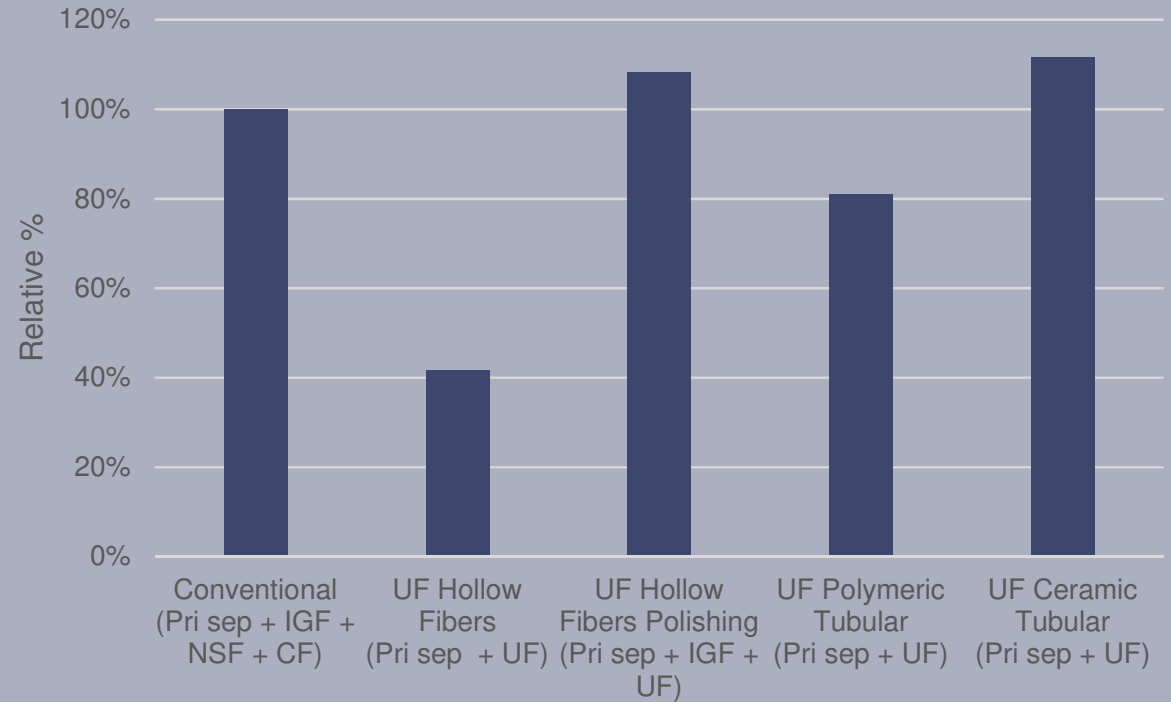
- Downstream technologies are less expensive (CAPEX wise) but with a higher footprint
- Membrane based lines are competitive CAPEX wise and OPEX wise, especially if there is a need for cartridge filtration, with an equivalent footprint
- Overall TCO is equivalent for upstream and downstream technologies
- Membrane-based technologies are all the more attractive when outlet specifications are tight

Cost evaluation for 60,000 m³/d

Relative CAPEX

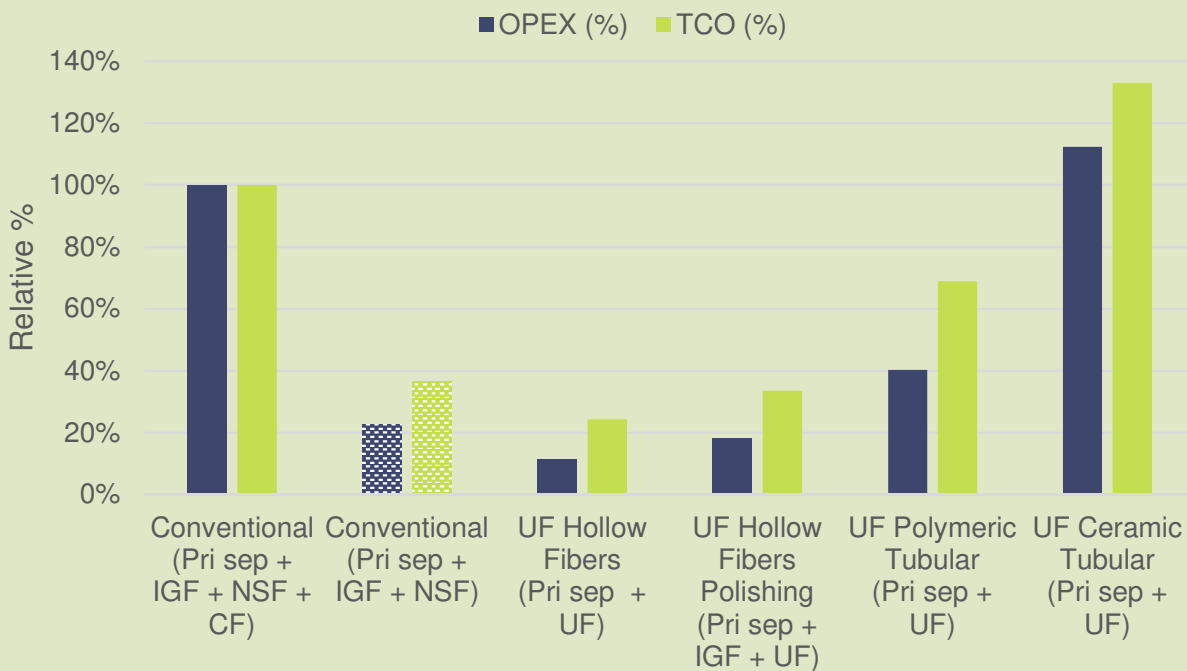


Relative Footprint



Footprint and main outcomes for 60,000 m³/d

Relative OPEX and TCO



At high flow:

- Tubular technologies are not competitive (CAPEX wise)
- Hollow Fiber technologies are competitive CAPEX wise and OPEX wise with an equivalent footprint when placed as a polishing step
- OPEX are low with membrane option due to cartridge replacement cost
- Overall TCO is higher for ceramic membranes but lower with polymeric membranes

Conclusion

Global Assessment and Conclusion

- Progression towards ZLD has seen emergence of new membrane technologies
- Suez investigation and testing program to find optimal configuration
 - Conventional Upstream & Downstream (CPI's, HC's, IGF/DNF, NSF, CF?)
 - Primary pre-treatment / advance polishing for satisfactory UF Membrane Life
 - Alternative (CPI's, HC's, UF)
 - Alternative advanced polishing (CPI's, HC's, IGF/DNF's, UF)

Global Assessment and Conclusion

- **Conventional – Robust and relatively competitive (if no requirement for CF)**
- **Tight Specs – UF competitive on CAPEX / OPEX / Footprint**
 - **Low Flows – Polymeric Tubular & Hollow Fibre best CAPEX / OPEX / Footprint**
 - **High Flows – Polymeric Hollow Fibre best CAPEX / OPEX / Footprint**
 - **Chemical and Temperature Resistance – Ceramic UF and/or Advanced Polishing Pre-treatment**
- **Consider all available technologies to treat water conditions / specs**

thank you

Acknowledgment

Special thank to Suez people who participated in this work: Emilie Sutton-Sharp and her team from the CIRSEE; Jocelyn Nadreau and his team from Poseïdon; Zac Moon and his team from SOGS; Cathy Fuchs and Antoine Coatalem from Industrial Solutions



Q&A

